# **Supporting Information**

## **Emissions from heated terpenoids present in vaporizable cannabis concentrates**

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**Figure S1.** Molecular structures of studied compounds



Figure S2. Integration of results from three different aerosol instruments to capture the mass range from 5 nm to 5  $\mu$ m. The figure shows the average particle number concentration measured with FMPS, OPS, and APS within the first minute of an experiment in which the full terpenoid mixture was heated at 500 °C.

**Table S1**. Mass concentration ( $\mu$ g/m<sup>3</sup>) of gas-phase terpenes measured by GC/MS in chamber air in the blank chamber and from evaporating the full terpenoid mixture at room (~25 °C) and elevated temperatures (100-500 °C). Reported values correspond to the average of duplicate **determinations.**



ND: Not detected

\*Determined with a single measurement.

**Table S2**. Mass concentration ( $\mu$ g/m<sup>3</sup>) of gas-phase terpenes measured by GC/MS in chamber air from heating the complex mixture, light fraction and heavy fraction mixture at 500 °C. Reported values correspond to the average of duplicate determinations.



ND: not detected

\* Values in italics correspond to concentrations of analytes that were not introduced in the tests, likely present as impurities of the released compounds and/or background chamber levels.

\*\* Determined with a single measurement.



**Figure S3**. Relative deviation of duplicate GC/MS measurements for each terpenoid in each of the three samples (A, B, and C) collected during experiments conducted at difference temperatures with the full terpenoid mixture. Relative deviation was calculated by dividing the absolute difference of two determinations by their average.



**Figure S4.** Relative deviation of the duplicate GC/MS measurements for each terpenoid in each of the three samples (A, B, and C) collected during experiments conducted with the complex mixture, light and heavy terpenoid mixtures at 500 °C. Relative deviation is calculated by dividing the absolute difference of the two values by their average.

**Table S3**. Mass concentrations of degradation byproducts  $(\mu g/m^3)$  in the chamber blank, and produced upon heating the full terpenoid mixture at different temperatures and heating the complex mix, full mix, light fraction and heavy fraction at 500 °C (blank subtracted). Reported results are the average of two simultaneous determinations, with the difference between those determinations reported in parenthesis.



ND: not detected

\* Average of two chamber blank measurements



**Figure S5.** Time series of chamber  $PM_{2.5}$ ,  $PM_{1.0}$ , and  $PM_{0.25}$  mass concentration ( $\mu$ g/m<sup>3</sup>) in all experiments, with the background concentration before the release of terpenoid mixture (time=0) subtracted from the data series. Inserts in the upper right corner show the difference between PM<sub>1.0</sub> and PM<sub>0.25</sub> mass concentration.



Figure S6. Contour plots of particle number (left) and mass (right) concentration distribution during the first 200 minutes after the full terpenoid mixture was delivered onto the heated surface.



Figure S7. Example of measured chamber O<sub>3</sub> concentration during the experiments, showing a very low level of O<sup>3</sup> present in the chamber before the release of terpenoids.



**Figure S8**. Time series of PM<sub>1</sub> mass concentration for aerosols formed from (A) heating the full terpenoid mixture at four different temperatures: 100, 250, 400, and 500 °C, and (B) heating at 500 °C four different mixtures: light fraction, heavy fraction, full mixture, and complex mixture. The plots include two versions of the full terpenoid mixture heated at 500 °C, calculated by assuming a particle density of 1 g/cm<sup>3</sup> and 0.9 g/cm<sup>3</sup>, respectively.



Figure S9. Particle mass concentration of aerosols within 8-200 nm diameter range, formed from heating the full terpenoid mixture at 500 °C. Calculated with (A) a particle density of 1  $g/cm^3$ ; and (B) with a particle density of  $0.9 \text{ g/cm}^3$ .

#### **Calculation of emission rates (***E***)**

The mass of acrolein, methacrolein and PM1.0 released into the chamber (*mi*), as well as the number of particles (*n*), were normalized by the mass of terpenoid mixture evaporated in chamber (*Mi*). The emission rate  $(E_i)$  for each contaminant *i* was determined by multiplying that ratio by the mass of terpenoids released per puff (*Mpuff*).

*(for acrolein, methacrolein and PM<sub>1.0</sub>)* 
$$
E_i = \frac{m_i}{M_i} \times M_{puff}
$$
 (1)

$$
E_i = \frac{n}{M_i} \times M_{puff}
$$
 (2)

The amount of terpenoids present in dabbing and vaping formulations, and the amount of VCC consumed per puff were both estimated from values reported in the literature. In the case of vaping, the predicted volume of e-liquid used in a vape-pen cartridge was 1 mL, and the fraction of terpenoids was between 5% and 20%, considering that in some cases terpenoids are not only present in the plant extract but also added as co-solvents.<sup>[1](#page-17-0)</sup> The predicted amount of e-liquid consumed per puff was between 30 and 70 µL. For dabbing, we used a mass of VCC consumed per dab of 40 mg, containing 6% of terpenoids[.](#page-17-1)<sup>2</sup> Consumption patterns change significantly from one device to the next, and also change from one user to another. The terpenoid content can also vary significantly. For these reasons, this approach is applicable to the study of different devices, concentrates and consumption patterns. The emission rates determined with equations S1 and S2 can be adjusted to reflect different product consumption rates and terpenoid compositions.

All calculations were based on chamber concentrations determined upon heating the full terpenoid mixture at 500 °C. Concentrations determined during the first 10 minutes (sample A) were used for this calculation. Dilution from air exchange, at  $0.2 h<sup>-1</sup>$ , was only 3% during the sampling period. The acrolein chamber concentration  $(0.4 \,\mu g \text{ m}^{-3})$  was comparable to that measured when the mixture was heated at 100, 250 and 400 °C. By contrast, the chamber concentration of methacrolein used in this analysis (2 µg m<sup>-3</sup>) was achieved after heating the full terpenoid mixture at 500 °C, but the compound was not present in emissions produced at lower temperatures. The PN and PM1.0 concentrations were averaged over the first hour after being released to the chamber.

#### **Calculation of daily users' intake**

The estimated daily intake for each compound (*DIi*) presented in Table 2 was calculated as:

$$
DI_i = E_i \cdot N \cdot R \tag{3}
$$

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where *N* is the number of daily puffs expected for average users, and *R* is the fraction retained by the user. In this calculation, we used a range of  $20 < N < 60$  for vaping, corresponding to a THC dosis equivalent to smoking between 1 and [3](#page-17-2) joints per day.<sup>3</sup> In the case of dabbing, it should be noted that on a recent survey of 869 US dab users, only half of respondents reported use frequency equal or higher than once per day. For those cases, we estimated  $2 < N < 6$  based on the reported mass of consumed concentrate[.](#page-17-3)<sup>4</sup> It should be noted that the number of daily puffs for cannabis vaping and dabbing was significantly lower than those reported for nicotine/PG/VG e-cigarettes (up to 2[5](#page-17-4)0 puffs per day)<sup>5</sup> and for conventional (tobacco) cigarettes (180-200 puffs per day for a moderately heavy smoker).<sup>[6](#page-17-5)</sup> In addition, all forms of cannabis consumption are reported with a lower proportion of daily users, compared to tobacco smokers[.](#page-17-6)<sup>7</sup>

#### **Calculation of the increment in pollutant concentrations (***ΔC***) in a home**

The amount of pollutant *i* released to the indoor environment per day  $(P_i)$  was calculated as

$$
P_i = E_i \cdot N \cdot (1 - R) \tag{4}
$$

The number of daily puffs (*N*) and fraction retained (*R*) were the same as those used to calculate the daily intake. The determined  $P_i$  values were used to calculate  $\Delta C$  as the 8-h average concentration in a 50-m<sup>3</sup> room with an air exchange rate of  $0.2 h<sup>-1</sup>$  following a dabbing or vaping event.

### **Calculation of the increment in pollutant concentrations (***ΔC***) in a public venue**

Results reported by Waring and Siegel (2006[\)](#page-17-7)<sup>8</sup> of the number of cigarettes smoked per hour by patrons in 17 smoking bars were used to predict the number of puffs per hour in a public venue, assuming comparable occupancy and product use rate. That study reported space volumes between 284 and 2508 m<sup>3</sup>, and the number of cigarettes consumed per hour between 40 and 130 units. The average number of cigarettes consumed per hour and per  $100 \text{ m}^3$  was 13. This factor was applied to predict the number of puffs per hour for vaping and dabbing in a public venue. In the case of vaping, we predicted 130 puffs per hour per  $100 \text{ m}^3$ , corresponding to 13 e-cigarettes consumed in that time frame at an average of 10 puffs per e-cigarette. For dabbing, 13 consumers at 2 puffs each were considered to predict a total of 26 puffs per hour per 100 m<sup>3</sup>. The amount released per hour and per 100 m<sup>3</sup> in each case was calculated with equation 4, and converted to concentrations in  $\mu$ g m<sup>-3</sup> (or to nr. of particles per cm<sup>3</sup>, in the case of PN). Table 2 reports  $\Delta C$  as the 8-h average concentration for an air exchange rate of 1 h<sup>-1</sup>, with vaping or dabbing taking place continuously during that period. The Waring and Siegel study reports a wide range of air exchange rates, between 0.6 and 6.5 h<sup>-1</sup>. Our chosen value of  $ACH = 1$  h<sup>-1</sup> represents the low end of that range.



**Table S4**. PN emission rates plotted in Figure 5



Figure S10. Particle emission rate (*E<sub>PN</sub>*) during the first 30 min for three different size bins: 5-50 nm, 50-100nm and 100-250 nm after heating (A) the full terpenoid mixture at different temperatures, and (B) different mixtures at 500 °C.

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