

1 **The implications of facility design and enabling policies on the economics of dry anaerobic digestion**

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10 **Abstract**

11 Diverting organic waste from landfills provides significant emissions benefits in addition to increasing
12 landfill capacity and creating value-added energy and compost products. Dry anaerobic digestion (AD) is
13 particularly attractive for the organic fraction of municipal solid waste because of its high-solids
14 composition and minimal water requirements. This study utilizes empirical data from operational
15 facilities in California in order to explore the key drivers of dry AD facility profitability, impacts of
16 market forces, and the efficacy of policy incentives. The study finds that dry AD facilities can achieve
17 meaningful economies of scale with organic waste intake amounts larger than 75,000 tonnes per year.
18 Materials handling costs, inclusive the disposal of inorganic residuals from contaminated waste streams
19 and post-digester mass (digestate) management, are both the largest and the most uncertain facility cost.
20 Facilities that utilize the biogas for vehicle fueling and earn associated fuel credits collect revenues that
21 are 4-6x greater than those of facilities generating and selling electricity and 10-12x greater than facilities

22 selling natural gas at market prices. The results suggest important facility design elements and enabling
23 policies to support an increased scale of organic waste handling infrastructure.

24 **Key words:** dry anaerobic digestion, high-solids anaerobic digestion, solid-state fermentation, renewable
25 natural gas, biofuel, organic waste management, landfill diversion

26 **List of Acronyms**

| | | |
|----|--------|---|
| 27 | AD | Anaerobic digestion |
| 28 | BioMAT | Bioenergy Market Adjusting Tariff |
| 29 | CHP | Combined heat and power |
| 30 | CI | Carbon intensity [cut?] |
| 31 | CNG | Compressed natural gas |
| 32 | GHG | Greenhouse gas |
| 33 | LCOD | Levelized cost of disposal |
| 34 | LCFS | Low Carbon Fuel Standard |
| 35 | MRWMD | Monterey Regional Waste Management District |
| 36 | O&M | Operations and maintenance |
| 37 | OFMSW | Organic fraction of municipal solid waste |
| 38 | RIN | Renewable Identification Number |
| 39 | RNG | Renewable natural gas |
| 40 | SI | Supplementary Information |
| 41 | SSFSC | South San Francisco Scavenger Company |
| 42 | SSO | Source-separated organics |

44 **1 Introduction**

45 Waste management activities, including landfills, wastewater treatment, and composting, were estimated
46 to account for 2% of U.S. greenhouse gas (GHG) emissions in 2016, based on the 100-year global
47 warming potential of the emissions (U.S. EPA, 2018a). The majority of these emissions occur when
48 organic waste decomposes anaerobically in landfills and produces methane (CH₄), a potent short-lived
49 climate pollutant (Duren et al., 2019). While landfill gas capture systems operate at approximately half of
50 U.S. landfills (U.S. EPA, 2020), these systems may only capture 66-88% of gases created over the
51 lifetime of the landfill (Barlaz et al., 2009). Prior life-cycle assessments agree that diverting organic waste
52 from landfills to waste-to-energy systems or composting achieves substantial net GHG emissions
53 reductions (Morris et al., 2013; Nordahl et al., 2020). In addition to the climate benefits, diverting the
54 organic fraction of municipal solid waste (OFMSW) from landfills also reduces the need to expand
55 landfill capacity, improves leachate quality (Jordan et al., 2020), and provides an opportunity to generate
56 renewable energy and recycle the organic material and nutrients back to the soil (Breunig et al., 2019).
57 These advantages of landfill diversion have motivated several large states and cities in the United States
58 (U.S.) to establish aggressive municipal solid waste (MSW) diversion goals, which will require extensive
59 build-out of organic waste handling infrastructure (Satchwell et al., 2018).

60 Anaerobic digestion (AD) facilitates the decomposition of organic waste in a controlled, oxygen-limited
61 environment and captures the resulting biogas (an approximately 50/50 mixture of CH₄ and CO₂) to
62 generate electricity or clean up and compress for use in pipelines or vehicles. AD also recovers nutrients
63 through the management of remaining solid digestate (Breunig et al., 2019). In the U.S., AD has
64 traditionally been used in the treatment of municipal wastewater (U.S. EPA, 2018b) and, increasingly, at
65 dairy farms (AgSTAR, 2018). While a small number of these traditional facilities accept municipal and
66 agricultural organic waste streams to co-digest with the human or animal wastes, new dedicated facilities

67 have been built in the U.S. within the last decade with the sole purpose of processing organic waste
68 diverted from landfills (Linville et al., 2015). Standalone AD of OFMSW presents challenges that are not
69 faced by wastewater treatment and dairy digester facilities, namely a highly variable feedstock, inorganic
70 contamination, and low moisture content relative to liquid wastes. Some of these challenges can be
71 mitigated through the use of dry AD (also known as high-solids or solid-state digestion) facilities that
72 process waste in their existing solid form, making dry AD of OFMSW a promising technology to meeting
73 landfill diversion, GHG emission, and renewable energy goals (Nordahl et al., 2020; Preble et al., 2020;
74 Satchwell et al., 2018). Dry AD is ideal for processing waste with solids content between 20 and 40%
75 (Rocamora et al., 2020). However, experiences from a growing set of dry AD facilities indicate that the
76 success of these facilities hinges on operational risks associated with mixed feedstocks, as well as the cost
77 of handling residual solids and the ability to monetize renewable energy outputs.

78 These technical and economic complexities make the long-term viability of dry AD facilities difficult to
79 predict. This work employs technoeconomic analysis to provide a comprehensive cost and revenue
80 analysis for dry AD facilities based on real-world data, covering a variety of technology and design
81 options. In a review of AD literature, Rajendran and Murthy (2019) found that environmental life-cycle
82 assessment papers vastly outnumber technoeconomic analysis, and existing technoeconomic analysis has
83 limited focus on OFMSW and no focus on dry or high-solids AD. Nordahl et al. (2020) conducted a deep-
84 dive into the environmental impacts of dry AD of OFMSW, including a comparison of bioenergy
85 utilization and digestate management pathways, but did not assess facility economics. Angelonidi and
86 Smith (2015) present operational and cost data from nine AD facilities in Europe, the majority of which
87 are high-solids or dry AD, but do not examine facility profitability or energy-related revenue streams.

88 Increasingly, systems optimization studies have incorporated wet or dry AD into the portfolio of assessed
89 technologies. Ascher et al. (2019) assessed wet AD with electricity generation and waste heat recovery
90 for management of organic waste in Glasgow, Scotland, and found that in order to be profitable, digestate
91 by-products must be sold or a carbon tax of at least \$140/tonne must be implemented. Waste tipping fees

92 were not considered in this study. Finally, Tominac et al (2021) examine the environmental impacts and
93 high-level economics (using a single dollars per tonne cost metric) of managing municipal organic waste
94 in Milwaukee, Wisconsin via landfill, compost, dry AD, and wet AD, with biogas being used to generate
95 electricity and digestate land-applied. Independent of tipping fee and specific facility siting and
96 transportation dynamics, they find that dry AD is preferred for 12% of organic waste. Economic analyses
97 have been conducted for wet AD of municipal solid waste, highlighting the dynamics between tipping
98 fee, energy revenue, and profitability (Rajendran et al., 2014; Sanscartier et al., 2012), but these studies
99 do not consider dry AD in particular, nor do they assess multiple energy utilization pathways, the cost of
100 disposing of post-AD solid digestate, or current bioenergy incentive frameworks in the U.S. Lastly, Khan
101 et al. (2016) found that a tipping fee of \$70-100 per tonne of waste was required for a dry AD facility to
102 earn an IRR of 10% in Alberta, Canada. In this analysis, only an electricity generation pathway was
103 examined, digestate management costs were not included, and modeled capital costs were significantly
104 lower than recently reported values.

105 This study is the first comprehensive technoeconomic analysis of dry AD facilities processing OFMSW,
106 using a new model with empirical data from operational facilities in California. The model is used to
107 determine the key cost and revenues, sources of uncertainty, and potential economic competitiveness with
108 landfills for dry AD across a wide range of facility scales and for three energy utilization pathways.
109 Careful attention is provided to specific policy and regulatory landscapes in California that impact costs
110 and revenues, and to factors that are of particular interest to dry AD facilities such as digestate
111 management.

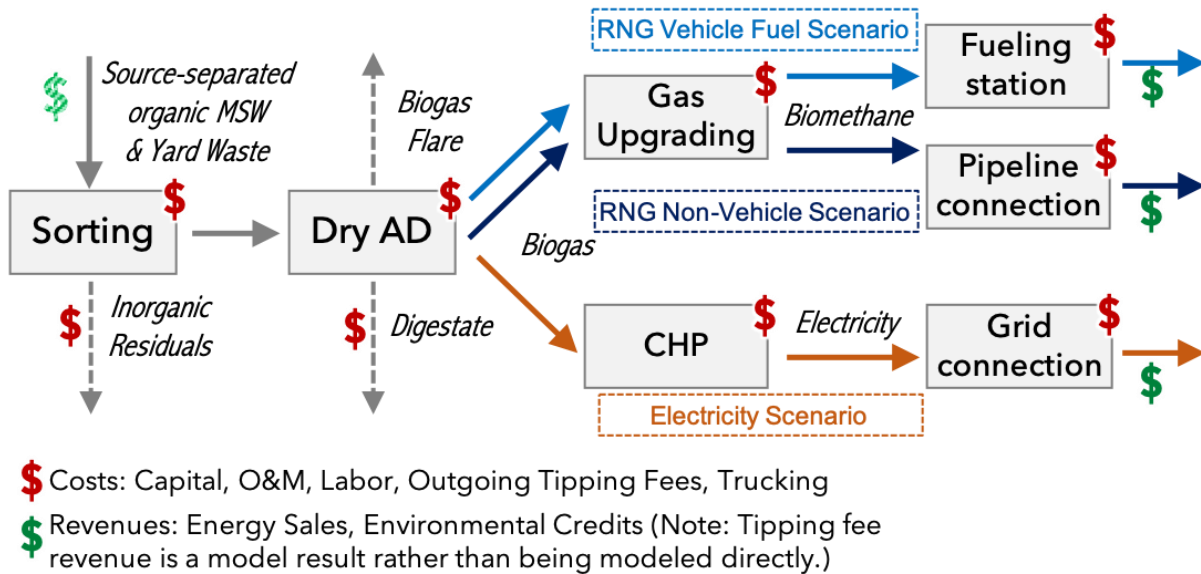
112 **2 Methods**

113 The dry AD economic model developed in this study calculates the annual costs and revenues of a
114 privately-owned dry AD facility over a 25-year lifetime (see Supplementary Information (SI) for details
115 on annual cash flow and discounting calculations). An overview of the modeling framework is shown in

116 Figure 1. A set of facility operational modeling equations, described in Section 2.1, determine the mass
117 and energy flows of the waste as it moves through sorting and digestion, and the generated biogas as it
118 moves from creation (in the digester) to the final energy delivery. Key assumptions for this analysis are
119 shown in Table 1. The model assesses three pathways for biogas utilization: (1) on-site combined heat
120 and power (CHP) generation using biogas (“Electricity scenario”), (2) upgrading biogas to pure methane,
121 referred to as renewable natural gas (RNG) or biomethane, and compressing for on-site vehicle fueling
122 (“RNG Vehicle Fuel scenario”), or (3) upgrading biogas to RNG for natural gas pipeline injection with
123 unspecified end-use (“RNG Non-Vehicle scenario”). Cost and revenues are calculated for each step in the
124 model, as denoted by the red and green dollar symbols in Figure 1 and described in Section 2.2. Capital,
125 operational, and labor costs are calculated for the sorting and digestion facility, the gas upgrading or
126 energy conversion equipment, and the energy delivery infrastructure. Trucking and disposal costs for the
127 inorganic residuals and post-digester digestate are also modeled. Revenues for a given energy product are
128 calculated based on current California market and policy incentive landscapes, while the revenue
129 associated with incoming waste into the facility (i.e., the tipping fee) is not modeled directly but is instead
130 an output of the model. Key cost parameters are shown in Table 2.

131 Model parameters rely in part on empirical data from full-scale operational facilities, particularly the Zero
132 Waste Energy Development Company (ZWEDC) facility in San Jose, California. Additional dry AD
133 facilities referenced include the Blue Line Transfer Inc. and South San Francisco Scavenger Co. (SSFSC)
134 digester in South San Francisco, California and the Monterey Regional Waste Management District
135 (MRWMD) digester in Monterey, California (see SI for a description of these facilities). The modeling
136 approach includes an uncertainty analysis to capture variations in potential facility performance (i.e.,
137 Low, Base, and High Performance scenarios) and uncertainty costs and revenue streams (i.e., Low, Base,
138 and High Cost scenarios; note that the Low Cost scenario contains both the lower bound of costs and the
139 upper bound of revenues, and vice versa for the High Cost scenarios). Facilities with rated digestion
140 capacity of 25,000 to 300,000 metric tonnes of wet waste (hereafter noted as tonnes) per year are modeled

141 to observe economies of scale. Though facility operations and cost categories and trends are
 142 generalizable, costs were modeled with a focus on California, and therefore other regions within the U.S.
 143 and globally may lie beyond our uncertainty ranges if feed-in tariffs, labor costs, and other market prices
 144 are dramatically different.



145
 146 *Figure 1. Model process flow diagram showing the major costs and revenues captured in the model for each of the three energy*
 147 *scenarios.*

148 **2.1 Facility Operations Modeling**

149 Table 1 shows the modeled assumptions, including ranges representing uncertainty, for key operational
 150 parameters, and Section 2 of the Supplementary Information provides more detail on parameters not
 151 described here. The facility modeled in this study accepts source-separated organics (SSO) from
 152 municipal residential and commercial sources and municipal yard waste. The level of contamination in
 153 SSO was assumed to be 40%, as reported by currently operating facilities; the facility employs manual
 154 sorting to remove 85% of the contamination, then mixes the SSO with yard waste in a 3-to-1 ratio (see
 155 SI). We assumed an average biogas yield of 85 standard cubic meters of biogas per wet metric tonne of
 156 waste (scm per tonne) and a range of 65 to 105 scm per tonne for the combined SSO and yard waste in the
 157 digester. Our base performance and bounded assumptions are consistent with assumptions used in recent

158 literature (Tominac et al., 2021) as well as empirical data on dry AD system biogas yields: the SSFSC and
 159 ZWEDC facilities in California reported 94-100 and 62-78 scm per tonne at, respectively, while
 160 Angelonidi and Smith (2015) report 78-90 scm per tonne for facilities in Europe that process mixed food
 161 and green waste and 50-106 scm per tonne for facilities with dry continuous systems. These biogas yield
 162 ranges depend on various digester design parameters such as feedstock moisture content, operating
 163 temperature, and retention time. We also assumed the generated biogas has a methane content of 55%
 164 (range 50-60%) by volume based on empirical facility data from ZWEDC and others (Angelonidi and
 165 Smith, 2015; Ong et al., 2014). The remaining portion is carbon dioxide (CO₂) with trace contaminant
 166 compounds.

167 *Table 1. Key operational parameter assumptions*

| Category | Base Performance | Upper and Lower Bounds Modeled | Units |
|--|------------------|--------------------------------|-----------------|
| Biogas yield | 85 | 65 - 105 | scm/tonne waste |
| Biogas methane content | 55 | 50 - 60 | % |
| Portion of biogas flared (CHP facilities) | 25 | 15 - 35 | % |
| Portion of biogas flared (biogas upgrading facilities) | 15 | 10 - 20 | % |
| Methane loss during biogas upgrading | 3 | 1 - 10 | % |
| CHP electrical efficiency | 40 | 36 - 44 | % |

scm = standard cubic meter, CHP = combined heat and power

168

169 **2.2 Facility Cost Modeling**

170 The residuals (i.e., inorganic contamination) separated from the waste once it reaches the AD facility
 171 must be landfilled; we estimated the cost of disposing residuals based on typical landfill tipping fees in
 172 California (see Table 2). California tipping fees are similar to the average tipping fees across the U.S. in
 173 terms of both the average and the range of values (CalRecycle, 2015; Environmental Research &
 174 Education Foundation, 2018). We assumed the cost of transporting the residuals to the landfill are
 175 negligible, as the total tonnage of inorganic contamination hauled out is small compared to other inbound
 176 and outbound tonnages, and digestion facilities are often co-located with landfills or other waste transfer

177 operations (e.g., as is the case for the observed facilities). A small portion of residuals will be recyclable,
178 but the monetary value of these materials, if any, is negligible based on our observations.

179 Digester capital costs were modeled using a standard exponential equation (see Table 2). The capital cost
180 equation for the base scenario was calibrated to the ZWEDC facility capital cost of \$43.5M (see SI for
181 details, including comparison to other reported facility costs). A scaling factor of 0.7 was assumed;
182 though wet AD facilities exhibit a scaling factor of 0.6 (Sanscartier et al., 2012), previously reported costs
183 of dry batch AD facilities appear to scale more linearly with facility capacity (Angelonidi and Smith,
184 2015). This is likely due to the fact that dry AD facilities, particularly those with batch processes, operate
185 multiple identical reactors in parallel and therefore do not exhibit the same economies of scale as simply
186 increasing the size of a wet AD tank. We assumed annual operating costs (not including labor) of 5% of
187 capital cost based on ZWEDC facility data. Gas upgrading costs (for removal of CO₂) for the RNG
188 energy utilization scenarios take a linear form, based on combined capital and operational costs from
189 European data collected from 2007-2008 (Ong et al., 2014). Labor was separated into three categories
190 (i.e., overhead, operations, and sorting) that scale differently with facility size and operational parameters
191 (see SI for assumptions). Annual employment costs, including employer-paid benefits, were based on
192 California-specific wage data (see Table 2; see SI for details).

193 *Table 2. Key cost assumptions*

| Cost Category | Base Cost | Upper and Lower Bounds Modeled | Cost Units |
|--------------------------------|--|---------------------------------------|--------------------|
| Residuals landfilling fee | 50 | 27 - 138 | \$/tonne residuals |
| Digester capital cost | $15,900 * (\text{tonnes/year capacity})^{0.7}$ | +/- 20% | \$ |
| Upgrading Capital + O&M | $444,000 + 0.18 * (\text{scm biogas})$ | +/- 20% | \$/year |
| Labor (total cost to employer) | 92,300 | +/- 20% | \$/FTE |
| Digestate trucking | 11 | 0 to +50% | \$/tonne digestate |
| Digestate disposal | 50 | +/- 33% | \$/tonne digestate |
| CHP capital | $13,150 * (\text{kW capacity})^{0.75}$ | +/- 30% | \$/engine |
| Electrical interconnection | 200,000 | 100,000-500,000 | \$/5 MW capacity |
| Electricity selling price | 100 | 60 - 127 | \$/MWh |
| CNG fueling station | 7 | +/- 25% | \$/MJ/d |
| CNG selling price | 0.015 | -10%; +30% | \$/MJ |

| | | | |
|-----------------------------|-------|---------|---------------------------|
| LCFS credit value | 150 | 100-200 | \$/tonne CO _{2e} |
| RIN (D5) value | 0.6 | +/- 50% | \$/RIN |
| Natural gas interconnection | 1 | 0.5 - 2 | \$M |
| Natural gas selling price | 0.003 | +/- 20% | \$/MJ |

CHP = combined heat and power; CNG = compressed natural gas; LCFS = Low Carbon Fuel Standard; RIN = Renewable Identification Number, FTE = full-time equivalent.

194

195 The AD process and subsequent short-term in-vessel composting cause a reduction in solid waste mass
196 (30%, according to ZWEDC tonnage reports) due to the transformation of solid mass into biogas as well
197 as loss of moisture. We modeled an arrangement where the facility pays to haul and dispose of digestate
198 at a third-party facility. For example, ZWEDC sends digestate to be composted off-site and other known
199 California AD facilities (i.e., SSFSC and MRWMD) also send their digestate for off-site management.
200 Base digestate trucking costs and tipping fees are based on ZWEDC’s actual costs. The low-cost scenario
201 assumes that facilities are co-located with compost operations, so trucking costs are negligible and tipping
202 fees were modeled as the California statewide median for yard waste at compost facilities. This is a
203 reasonable lower bound given that digestate from facilities processing mixed organic waste will be more
204 heterogeneous and contaminated than yard waste, so fees would likely be higher to reflect the
205 management challenges posed by moisture, odor, and inorganic contamination (Cotton, 2019).

206 2.2.1 Electricity Generation

207 Assumptions regarding the combined heat and power (CHP) equipment efficiency and costs are described
208 in the SI. There are various arrangements under which dry AD facilities can sell electricity in California
209 for a premium (see compensation assumptions in Table 2). The highest price typically achievable is
210 through the state’s Bioenergy Market Adjusting Tariff (BioMAT) program, which for municipal waste
211 digesters is currently \$127 per MWh (CPUC, 2018). This price is multiplied by a seasonal- and time-of-
212 day-varying factor that represents the value of the electricity to the grid, but we assumed facilities do not
213 have long-term biogas storage or excess generator capacity and therefore generate roughly constant power
214 output on average. If unable to enroll in the BioMAT program, a facility could at a minimum obtain a
215 wholesale price for electricity, which generally ranges from \$40-60 per MWh in California (U.S. Energy

216 Information Administration, 2019), plus any value from renewable energy credits. A third option is to
217 enter a power purchase agreement with an individual energy consumer or aggregator; examples of this
218 have been seen at wastewater treatment plant digesters in California. For example, East Bay Municipal
219 Utility District sells power directly to the neighboring port of Oakland for \$58 per MWh (Hake et al.,
220 2017), while Central Marin Sanitation Agency has a power purchase agreement with Marin Clean Energy,
221 a municipal energy aggregator, for approximately \$105 per MWh (CMSA, 2018).

222 2.2.2 RNG Vehicle Fuel

223 For the RNG Vehicle Fuel scenario, the facility pays to construct and maintain a fueling station to sell
224 renewable compressed natural gas (sometimes referred to as R-CNG, where the vehicle fuel more
225 broadly, including from fossil resources, is referred to as CNG). RNG is sold (or self-consumed) at a
226 value equal to current California fossil CNG fuel prices, and the facility is eligible for both state and
227 federal renewable fuel incentives.

228 California's Low Carbon Fuel Standard (LCFS) awards credits based on the carbon intensity (CI) of the
229 renewable fuel, calculated on a facility-by-facility basis with a limit on the GHG credit a facility can
230 incorporate based on avoided landfill methane emissions (California Air Resources Board, 2018;
231 Schwarzenegger, 2007). Two dry AD facilities are currently certified through the LCFS system; the
232 SSFSC facility, which processes a mix of food and yard waste, has a CI of -22.93 gCO₂-eq per MJ, while
233 a southern California facility digesting only yard waste is certified at a CI of 0.34 gCO₂e per MJ
234 (California Air Resources Board, 2019a). Assuming a conservative CI of -10 gCO₂e per MJ for the AD
235 facility, the resulting fuel would earn credits at a rate of 104 g CO₂e per MJ of fuel (California Air
236 Resources Board, 2019b). Historically, credit prices have varied from \$20 to 120 per tonne CO₂e
237 mitigated, but from July, 2018 to August, 2020 they have consistently hovered near the ceiling price of
238 \$200 per tonne CO₂e (California Air Resources Board, 2020). Future credit amounts and market
239 conditions leave significant uncertainty in the long-term price and, therefore, we model LCFS credit
240 prices of \$100-200 per tonne CO₂e.

241 Federal Renewable Fuel Standard credits, called Renewable Identification Numbers (RINs), are earned
242 for every 77,000 Btu (81 MJ) of fuel produced. We conservatively used “D5” market prices in this
243 analysis, which is the credit type currently available for dry AD facilities processing OFMSW, though
244 there has been much contention surrounding the qualifying category of credits (Greene, 2017; Pleima,
245 2019). The regulatory floor and ceiling price for D5 RINs is \$0.05 and \$2.00 per RIN, respectively, and
246 while prices have varied over the last 10 years between \$0.15-1.15 per RIN, they have remained below
247 \$0.50 per RIN since late-2018 (U.S. EPA, 2019).

248 2.2.3 RNG Non-Vehicle (Pipeline Injection)

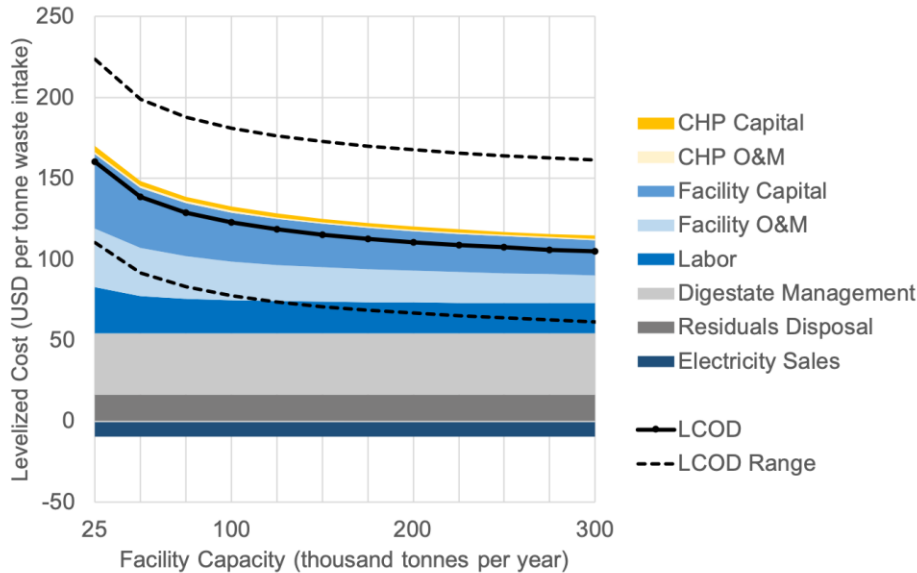
249 The RNG Non-Vehicle scenario assesses the economics of injecting RNG into the natural gas grid for
250 generic, untracked usage. In this case, the facility must invest in a pipeline interconnection station and
251 will receive revenues in line with wholesale natural gas prices. Sales were assumed to occur at wholesale
252 natural gas prices, which are typically \$0.003-0.006 per MJ; in 2017 the California average selling price
253 was \$0.003 per MJ (U.S. Energy Information Administration, 2019). There is currently no option for
254 monetizing the environmental benefits of pipeline-injected, end-use-agnostic RNG at a state or federal
255 level. In late 2018, the California legislature passed a bill authorizing the state utilities commission to
256 develop a biomethane procurement program, which in theory will raise the market value of pipeline-
257 injected biomethane (California Senate, 2018). However, the scope and timeline of this bill is unknown
258 and therefore we did not include any above-market revenues for biomethane in this scenario.

259 3 Results and Discussion

260 Our results are reported on the basis of the levelized cost of disposal (LCOD), which can be thought of as
261 analogous to the often-used levelized cost of energy (Ayres et al., 2004). LCOD represents the per-tonne
262 tipping fee the facility would need to receive to achieve a net present value of zero (i.e., the facility earns
263 a rate of return equal to the discount rate). Figure 2 shows the key costs and drivers for an AD facility
264 under the Electricity scenario. Costs are reported per tonne of wet waste delivered to the facility, levelized

265 over the 25-year lifetime of the facility. The net of these costs therefore represents the LCOD (black line
266 in Figure 2). The dashed lines in Figure 2 represent the upper and lower bounds of LCOD across cost and
267 performance scenarios. Results suggest economies of scale, as the LCOD for the smallest facility
268 analyzed here (25,000 tonnes of waste intake per year) is approximately \$160 per tonne (range \$110-223),
269 more than 50% higher than the largest facility (300,000 tonnes of waste intake per year; LCOD \$105 per
270 tonne with range \$60-160). These economies of scale primarily occur in the capital, labor, and O&M
271 categories; half of the potential economies of scale shown are realized at a facility size of 75,000 tonnes
272 per year, with decreasing cost reductions at larger sizes. There is a tradeoff in transportation costs
273 associated with sourcing waste from a larger area to achieve these economies of scale. However, the role
274 that waste hauling costs plays in the LCOD is complicated by the fact that waste collection and hauling
275 services may be provided by one or more separate entities (as is the case for the ZWEDC facility), each
276 with their own contracts and cost structures.

277 Baseline costs for a 100,000 tonne-per-year AD facility under three energy production scenarios are
278 shown in Figure 3. LCOD is highest for the RNG Non-Vehicle scenario at \$140 per tonne (range \$102-
279 195), due to the low value of the RNG as a replacement for natural gas, the absence of policy incentives,
280 and the biogas upgrading costs incurred by the facility. Electricity-generating facilities are less expensive
281 than RNG Non-Vehicle facilities at \$123 per tonne (range \$78-181). The RNG Vehicle Fuel scenario has
282 a baseline LCOD of \$105 per tonne. The RNG Vehicle Fuel scenario's lower bound is estimated at \$32
283 per tonne, significantly lower than the other scenarios, due largely to revenue from California state and
284 U.S. Federal incentives for renewable transportation fuels (LCFS and RINs), although the upper end of
285 the LCOD range is similar to other scenarios at around \$178 per tonne.



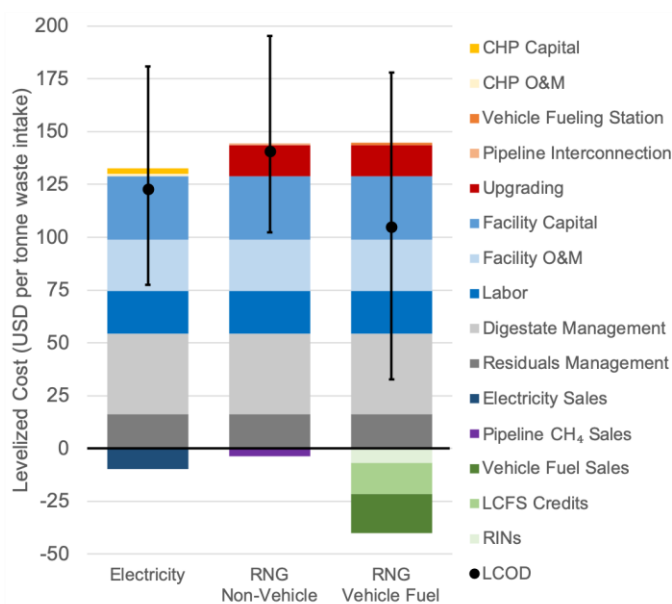
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287 *Figure 2. Levelized costs and revenues for a facility over a range of sizes operating under the Electricity scenario. Lines show*
 288 *the net costs, or the levelized cost of disposal (LCOD). Cost and revenue areas and long dashed line represent the Base*
 289 *Performance, Base Cost scenario, while smaller dashed lines show the range of LCOD values under all performance and cost*
 290 *scenarios.*

291 In all cases, the largest cost on a per-tonne basis is the management of the digestate (26-29% of facility
 292 costs), which includes costs for third-party digestate transportation and management. Of the organic waste
 293 loaded into the digester, approximately 70% of the original mass remains in the solid digestate. Combined
 294 with the cost of disposing of inorganic residuals, (11-12% of costs), the final disposal of waste streams
 295 from the facility accounts for 40% of operating costs. This outweighs even the capital costs of building
 296 the digester (21-23% of costs) and upgrading the gas to methane in the RNG scenarios (10%). The role of
 297 solid waste management and disposal in facility economics is a motivator for recent efforts to develop
 298 alternative treatments for digestate, such as pyrolysis, which can produce additional energy (syngas), soil
 299 amendments (biochar), and/or bio-oil that can be recycled into the digester (Liu et al., 2020; Monlau et
 300 al., 2016).

301 Energy revenues vary across the three scenarios. In the RNG Non-Vehicle scenario, gas is sold at
 302 wholesale prices earning ~\$2-6 per tonne of waste. This revenue is insufficient to offset the cost of
 303 upgrading the biogas to biomethane (~\$14 per tonne waste). At the low end of power output and feed-in
 304 tariffs, revenue from electricity generation is similarly low at \$3 per tonne of waste (as modeled in the

305 Low Performance-High Cost scenario). At the upper end of potential power generation and feed-in tariffs,
 306 revenue from electricity sales can reach \$21 per tonne waste, while the Base Performance-Base Cost
 307 scenario yields approximately \$10 per tonne waste. The comparative costs and revenues across energy
 308 utilization pathways are applicable beyond dry AD, to any biogas-generating facility including
 309 wastewater treatment plants and stand-alone wet AD, though metrics per tonne of waste will vary due to
 310 the impact of waste composition, moisture, residence time, and other operational parameters on biogas
 311 yields.

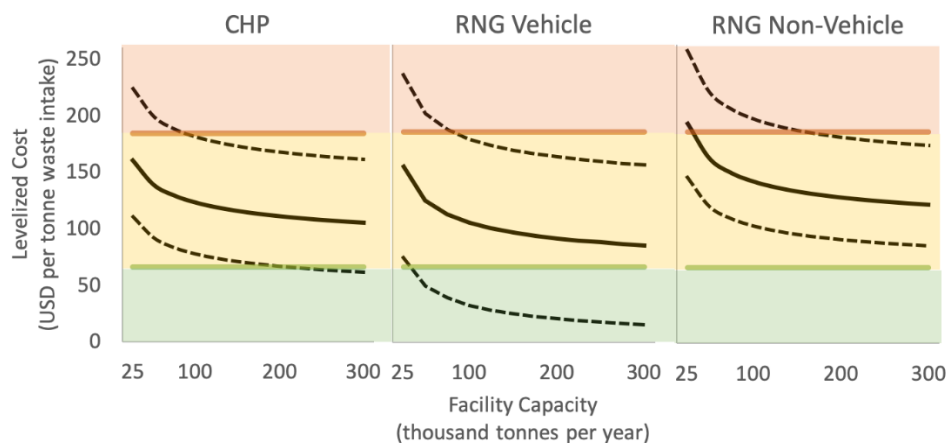


312
 313 *Figure 3. Per-tonne costs and revenues by category for a 100,000 tonne-per-year facility under three energy production*
 314 *scenarios. The stacked bars and dots represent the costs and revenues for the base operation and medium costs scenario, while*
 315 *the error bars represent the range of LCOD values across all operation and cost scenario combinations.*

316 3.1 Competitiveness with landfills

317 Landfilling is the most prevalent OFMSW disposal alternative to AD, as compost facilities do not
 318 commonly handle OFMSW due to contamination levels and concerns about odors and pests (Cotton,
 319 2019). Hence, the LCOD results in this study can be contextualized through a comparison with landfill
 320 tipping fees adjusted to represent a lifetime average comparable to LCOD (denoted as LCOD-equivalent;
 321 see SI for adjustment calculations). Tipping fees across California vary from \$0 to 184 per tonne of waste
 322 (LCOD-equivalent); zero values arise when landfills are county-owned and paid for through non-tipping-

323 fee revenue mechanisms such as property taxes (see Figure S2) (CalRecycle, 2015). Landfill tipping fees
 324 vary across the United States, with average LCOD-equivalents exceeding \$100 per tonne in small, land-
 325 constrained states in the Northeast (e.g. Rhode Island, Delaware), Hawaii, and Alaska (see Figure S2)
 326 (Environmental Research & Education Foundation, 2018). Figure 4 compares the California median
 327 landfill LCOD-equivalent of \$66 per tonne and the maximum of \$184 per tonne to modeled LCOD for
 328 dry AD. A facility with LCOD in the orange zone of Figure 4 would not be competitive with any landfill
 329 in the state, while the yellow zone represents competitiveness with the more expensive landfills in the
 330 state and the green zone corresponds to competitive costs relative to a majority of state landfills.
 331 Compared to a \$66 per tonne LCOD-equivalent, the RNG Vehicle Fuel and Electricity scenarios could be
 332 competitive if facilities achieve lower-than-expected costs, but the scale required to make the Electricity
 333 scenario competitive (225,000 tonnes per year) is beyond the largest dry AD facilities currently in
 334 operation. If compared to \$184 per tonne, which is the highest tipping fee in California and near the upper
 335 end in the U.S., AD facilities are far more likely to be competitive. Specifically, at this \$184 per tonne
 336 landfill tipping fee equivalent, assuming waste intake greater than 100,000 tonnes per year ensures that
 337 the Electricity and RNG Vehicle Fuel scenarios will be economically attractive. In more populated areas,
 338 reaching this scale will be possible (even if waste is hauled no more than 20 km), while smaller cities and
 339 rural areas will need to aggregate their wastes at centralized facilities (Scown et al., 2019).



340

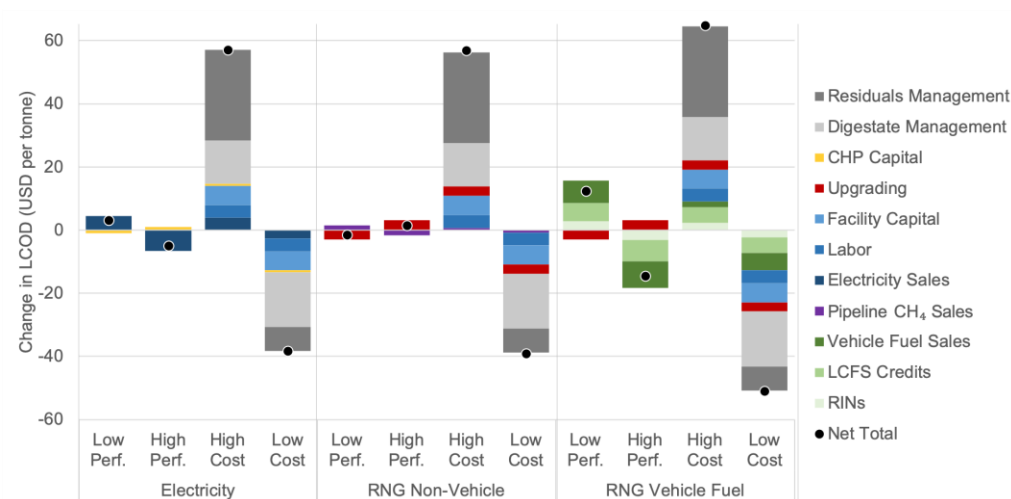
341 *Figure 4. Economic competitiveness of AD facilities with landfills across a range of capacities (x-axis) and energy scenarios*
342 *(panels). LCOD of AD for the base case (solid black line) and uncertainty range (dashed lines) are compared to the median*
343 *(green line) and maximum (orange line) LCOD-equivalent landfill tipping fee in California.*

344 Although outside of the scope of this analysis, it is worth noting that source-separation and/or pre-
345 processing required to reduce contamination levels to levels acceptable for dry AD can result in additional
346 costs. These costs may be in the form of separate bins and collection routes to facilitate increased source-
347 separation or in processing at materials recovery facilities that are designed for high organics recovery
348 (e.g., using de-packaging machines). Some of the costs and benefits of diverting organic waste from
349 landfills are not monetized in this analysis, including the conservation of existing landfill capacity,
350 reduction in landfill biogas generation, improvement in leachate quality, potential recovery of organic
351 matter and nutrients, and changes in GHG and other air pollutant emissions (Chen et al., 2021; Morris et
352 al., 2013; Nordahl et al., 2020). However, estimated social costs of landfilling wet organic waste based on
353 the impacts of air pollutant and greenhouse gas emissions are \$25-40 per tonne according to results from
354 a recent life-cycle assessment of dry AD (Nordahl et al., 2020). If these costs were incorporated into
355 landfill tipping fees, it would increase the relevant point of comparison and make AD facilities
356 competitive at even more sizes and configurations.

357 **3.2 Uncertainty**

358 The LCOD can vary by more than \$60 per tonne within the range of cost and performance scenarios we
359 analyzed (see Figure 5). Unit costs drive the majority of the uncertainty, while the variations in facility
360 performance do not have as large an impact on LCOD. In all cases, the cost of managing inorganic
361 residuals and solid digestate is single largest source of uncertainty, accounting for a -\$25 to \$42 per tonne
362 variation in LCOD. If residuals and digestate costs were held constant at the Base Cost values, the overall
363 LCOD uncertainty range for 100,000 tonne-per-year facilities would shrink by 65%, 73%, and 46% for
364 the Electricity, RNG Non-Vehicle, and RNG Vehicle Fuel scenarios, respectively (see Figure S3 for
365 comparison). In the High Performance scenarios, costs increase due to the need to process (i.e., combust
366 or upgrade) additional biogas. In the Electricity and RNG Vehicle scenarios, the revenues from increased

367 energy production outweigh this cost, but in the RNG Non-Vehicle-High Performance scenario the
 368 additional market gas revenues are smaller than the additional gas upgrading costs, resulting in a net
 369 increase in LCOD.



370

371 *Figure 5. Variation in LCOD caused by individual factors for a 100,000 tonne-per-year facility under various scenarios as*
 372 *compared to the base operation-base cost scenario for the given fuel pathway. The Low and High Performance (Perf.) scenarios*
 373 *retain the Base Cost assumptions, while the Low and High Cost scenarios retain the Base Performance assumptions. Results for*
 374 *combinations of these scenarios (e.g. High Performance-High Cost) would be additive, but not linearly so. Cost categories with*
 375 *less than a 1% impact on LCOD across all scenarios have been removed from the figure for clarity.*

376 Although a wide range of costs are covered in our uncertainty analysis, facilities outside of California
 377 may have costs outside of that range, particularly labor costs in much of the U.S. would likely be lower
 378 than our modeled range. (Bureau of Labor Statistics, 2019). Digestate management costs may also be
 379 lower in areas with inexpensive land, where odor is not a concern, and with different regulations
 380 governing the year-round composting or land application. It should also be noted that, while the LCFS is
 381 specific to California (a number of other states do have variations of this policy in place), facilities outside
 382 of California are eligible to earn LCFS credits if they sell into the California market.

383 3.3 Energy prices and policy impacts

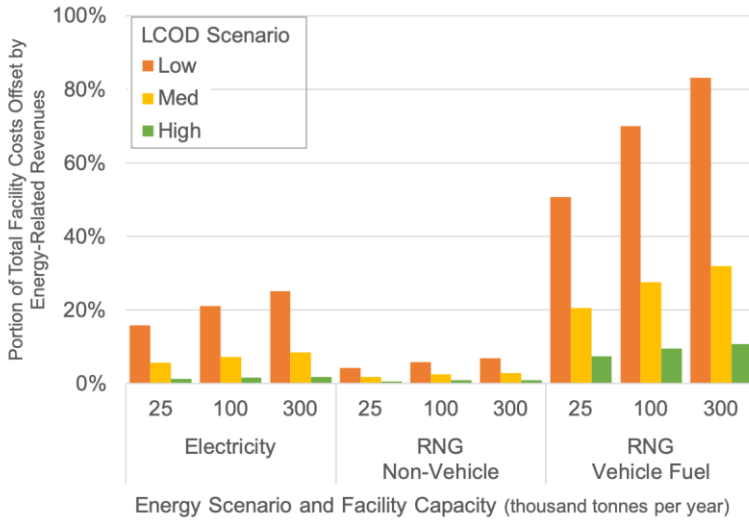
384 The wholesale market value of energy outputs from AD facilities, absent any policy incentives, is a minor
 385 source of revenue relative to what is required to offset facility costs, as highlighted in the RNG Non-
 386 Vehicle scenario where gas pipeline revenues offset 1-7% of facility costs. If the facility can earn retail

387 energy prices instead of wholesale prices, as is the case for the RNG Vehicle Fuel scenario, these energy
388 revenues can offset 4-37% of costs. However, participation in the vehicle fuel market is predicated upon
389 the ability to find reliable customers, ideally a fleet of medium- or heavy-duty vehicles, which may be
390 difficult for facility owners who do not own related businesses such as a waste hauling fleet, or facility
391 locations that are not close to a major road network. Adjacent investment decisions such as whether to
392 convert a trucking fleet from diesel to CNG are outside the scope of the model, but it is worthwhile to
393 note that the availability of CNG customers can factor into a facility's decision to pursue this option. In
394 the Electricity scenario, policies such as renewable feed-in tariffs or power purchase agreements valued
395 above wholesale prices can increase energy revenues, though the total value relative to the costs is at most
396 25%. The combination of the facility's ability to capture retail revenues paired with substantial state and
397 federal incentive programs make the RNG Vehicle Fuel scenario the lowest-cost option from an LCOD
398 perspective. However, these increased revenues are uncertain, varying by a factor of 5 across the cost
399 scenarios modeled, because fuel credits trade on an open market and therefore future prices will fluctuate.

400 The less money a facility earns through energy sales and related incentives, the more they must earn
401 through tipping fees in order to be financially viable. The relative importance of these two revenue
402 streams may impact the way the facility is built and operated. Figure 6 shows the share of total revenues
403 that comes from energy sales and energy-related incentives in each scenario assuming an operational
404 facility earns a tipping fee required to break-even (i.e., commensurate with the LCOD). Energy is
405 responsible for at most 7% of revenues in the RNG Non-Vehicle scenario, while the Electricity scenario
406 earns 15-25% of revenues from energy at the high end, depending on facility size. In these cases, the
407 facility would be less motivated to invest in improving energy generation processes such as optimizing
408 gas yield or reducing flaring, as their money would primarily come from waste intake. Conversely, if
409 energy is the dominant revenue source (up to 83% in the RNG Vehicle Fuel scenario), the facility may be
410 motivated to maximize energy output and become selective in the waste they accept in an effort to
411 generate as much gas as possible. This could limit the diversion opportunities for more contaminated or

412 difficult-to-handle streams such as mixed municipal solid waste. Energy and waste policy planners should
413 carefully consider the prices being offered from various sources and what it will mean for both waste
414 disposal costs as well as drivers for facility operation and investment. Additionally, regulations could be
415 put in place on the way facilities operate (e.g., minimum retention times, best practices for percolate
416 circulation) and acceptable waste streams in order to ensure that facilities being supported by public
417 policies and money are operating in a way that maximizes their social benefits.

418 New energy-related value streams could be considered to ensure that AD facilities are incentivized to
419 maximize their energy and emissions benefits. For example, electricity-generating facilities offer a
420 dispatchable form of renewable energy and therefore could be incentivized to follow specific dispatch
421 schedules that help meet peak demand and ramping needs of the grid. The current BioMAT program in
422 California accomplishes this to a limited extent through time-of-day modifying factors. The same grid
423 benefits could be achieved by injecting RNG into natural gas pipelines for use at off-site facilities, but this
424 scenario is currently the least economically viable. New monetization mechanisms for RNG used in non-
425 vehicle fuel purposes could open up opportunities to reduce the carbon footprint of existing natural gas
426 power plants and decarbonize industrial processes that are too difficult or expensive to electrify, either
427 through co-location with an AD facility for direct biogas combustion and/or heat recovery from CHP
428 units or through direct sales via the natural gas grid. These added revenues would also lower the LCOD of
429 AD facilities and make them economically viable at lower tipping fees.



430

431 *Figure 6. Share of revenues coming from energy sales and incentives under a breakeven scenario, where the facility is earning a*
 432 *tipping fee equal to the levelized cost of disposal (LCOD), for three energy scenarios and three facility sizes over the range*
 433 *LCOD uncertainty (low, medium, high).*

434 **4 Conclusions**

435 Dry AD facilities are a financially viable approach to help meet landfill diversion and renewable energy
 436 goals, though organic and inorganic waste management costs are significant and uncertain (+/- 30-70% of
 437 baseline LCOD depending on scenario). Depending on alternative disposal options and local landfill
 438 tipping fees, dry AD may be cost-competitive under existing policies and energy prices or may require
 439 additional support through guaranteed higher tipping fees, subsidized materials handling costs, or new
 440 and increased energy-related monetary incentives. Each of these strategies incentivize different
 441 investments and behavior by owners and operators, and should, therefore, be considered carefully.

442 Economies of scale are important to the overall LCOD. The largest facilities we modeled (i.e., 300,000
 443 tonnes per year) generally had LCOD values that were 55-70% those of the smallest facilities we modeled
 444 (i.e., 25,000 tonnes per year). However, larger facilities may face barriers not explicitly considered in this
 445 study such as difficulty obtaining feedstocks from local sources, odor and emissions management issues,
 446 and resistance from neighboring communities. Materials handling costs, namely the disposal of inorganic
 447 residuals that come into the facility and the management of post-AD digestate by third-party composters,

448 vary considerably and have the potential to be well over half of the total per-tonne costs incurred by a
449 facility. However, some of the uncertainty can be mitigated through materials contracts and holistic waste
450 management policy support.

451 RNG for use as a vehicle fuel is currently the most lucrative energy utilization pathway for AD facilities
452 due to existing U.S. Federal and state policy incentives. Upgrading the biogas to RNG for non-vehicle
453 fuel uses is not economically attractive, as the upgrading costs alone outweigh wholesale natural gas
454 revenues and no economic incentives currently in place to support the production of RNG for non-vehicle
455 applications. Lastly, electricity generation is an economically viable pathway in cases where the
456 alternative landfill tipping fees are high, and may be attractive for facilities that do not operate truck fleets
457 capable of utilizing RNG and cannot easily connect to natural gas pipelines. Advanced electricity dispatch
458 strategies and monetization of thermal energy from combined heat and power units could help make this
459 scenario more attractive.

460 Limitations of the study include significant focus on the physical, financial, and operational
461 characteristics of a specific facility in California and use of deterministic inputs as opposed to an
462 operational framework that determines facility size, operations and costs to achieve a specific financial or
463 operational objective (e.g., least cost, specific return on investment). Dry AD technology is still quite
464 nascent in the U.S. and we have limited empirical data to draw from for inputs and assumptions. While
465 this study used bounding assumptions to represent uncertainty, public data on dry AD facility financial,
466 operating, and production characteristics would generate more precise results. Opportunities for future
467 technoeconomic analysis of dry AD facilities include additional consideration of byproduct management
468 pathways such as novel composting methods, land application of raw material, or pyrolysis of digestate,
469 as well as any associated revenues from the sale of finished compost or biochar (a byproduct of
470 pyrolysis). Future studies could also quantify the benefits of various levels of RNG- and thermal energy
471 recovery- related economic incentives and opportunities for co-location with other industrial facilities that
472 can utilize a range of energy byproducts. As more dry AD facilities are built and more data becomes

473 available, research should further explore the impact of facility design parameters such as digester
474 residence times, gas storage capacity, and feedstock composition on the costs and benefits, as well as the
475 societal impacts, of dry AD.

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